

# *Overview*

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## **Classical PID Control** *(continuous-time)*



This lecture recalls and examines a particular control structure that has become almost universally used in industrial control. It is based on a particular fixed structure controller family, the so-called **PID controller** family. These controllers have proven to be robust and extremely beneficial in the control of many important applications.

PID stands for:

- P** (*Proportional*)
- I** (*Integral*)
- D** (*Derivative*)



# PID Structure

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Consider the simple SISO control loop shown in Figure 6.1:

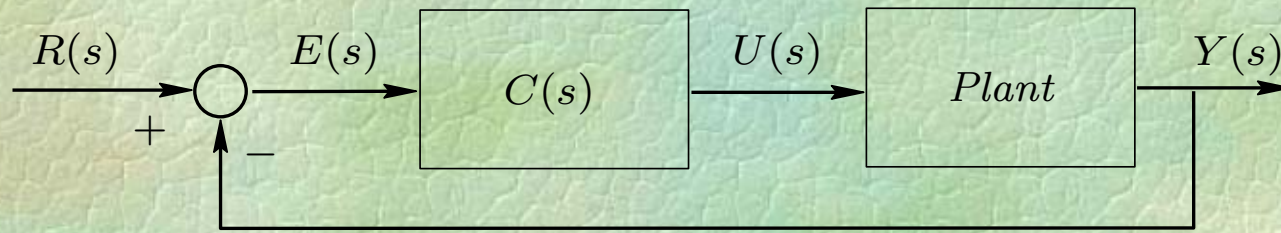


Figure 6.1: *Basic feedback control loop*



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The *standard form* PID are:

*Proportional only:*  $C_P(s) = K_p$

*Proportional plus Integral:*  $C_{PI}(s) = K_p \left( 1 + \frac{1}{T_r s} \right)$

*Proportional plus derivative:*  $C_{PD}(s) = K_p \left( 1 + \frac{T_d s}{\tau_D s + 1} \right)$

*Proportional, integral and derivative:*  $C_{PID}(s) = K_p \left( 1 + \frac{1}{T_r s} + \frac{T_d s}{\tau_D s + 1} \right)$



# Tuning of PID Controllers

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Because of their widespread use in practice, we present below several methods for tuning PID controllers. *Actually these methods are quite old and date back to the 1950's.* Nonetheless, they remain in widespread use today.

In particular, we will consider the:

- x *Ziegler-Nichols Oscillation Method*



# Ziegler-Nichols (Z-N) Oscillation Method

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This procedure is only valid for open loop stable plants and it is carried out through the following steps

- x Set the true plant under proportional control, with a very small gain.
- x Increase the gain until the loop starts oscillating. Note that linear oscillation is required and that it should be detected at the controller output.



- x Record the controller critical gain  $K_p = K_c$  and the oscillation period of the controller output,  $P_c$ .
- x Adjust the controller parameters according to Table 6.1 (*next slide*); there is some controversy regarding the PID parameterization for which the Z-N method was developed, but the version described here is, to the best knowledge of the authors, applicable to the parameterization of standard form PID.



**Table 6.1:** *Ziegler-Nichols tuning using the oscillation method*

	$K_p$	$T_r$	$T_d$
<b>P</b>	$0.50K_c$		
<b>PI</b>	$0.45K_c$	$\frac{P_c}{1.2}$	
<b>PID</b>	$0.60K_c$	$0.5P_c$	$\frac{P_c}{8}$



# Numerical Example

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Consider a plant with a model given by

$$G_o(s) = \frac{1}{(s+1)^3}$$

Find the parameters of a PID controller using the Z-N oscillation method. Obtain a graph of the response to a unit step input reference and to a unit step input disturbance.



# Solution

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Applying the procedure we find:

$$K_c = 8 \quad \text{and} \quad \omega_c = \sqrt{3}.$$

Hence, from Table 6.1, we have

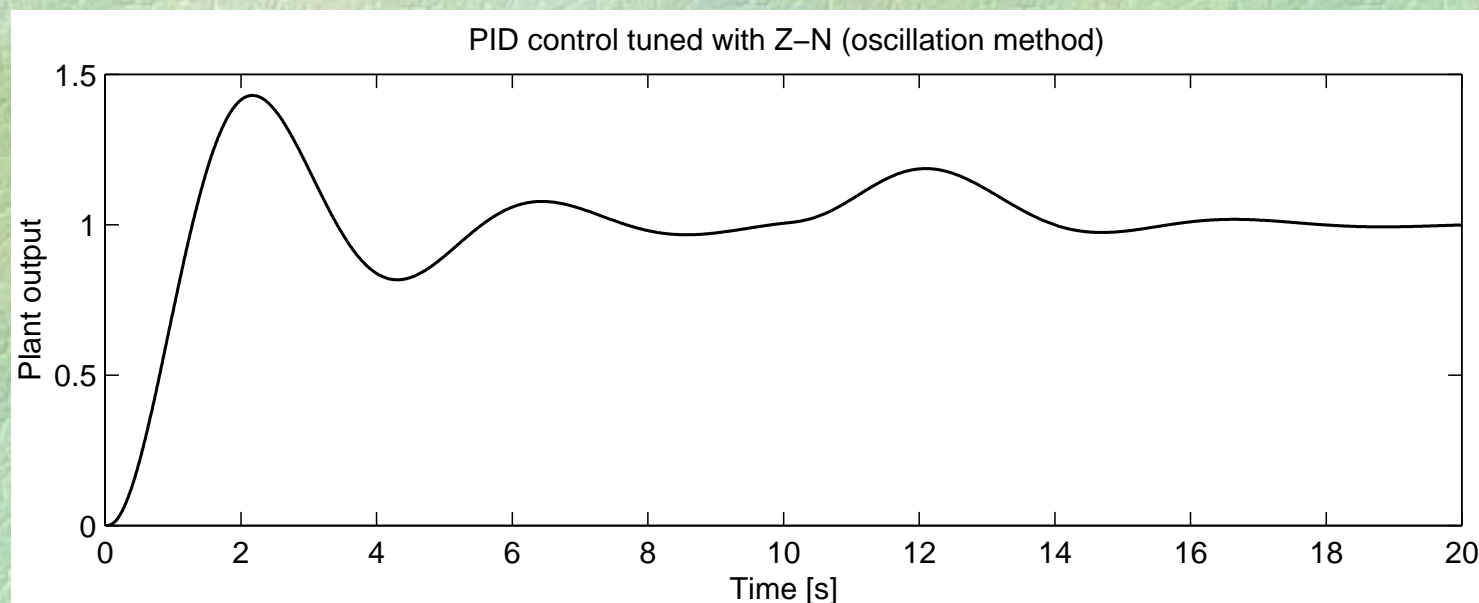
$$K_p = 0.6 * K_c = 4.8; \quad T_r = 0.5 * P_c \approx 1.81; \quad T_d = 0.125 * P_c \approx 0.45$$

The closed loop response to a unit step in the reference at  $t = 0$  and a unit step disturbance at  $t = 10$  are shown in the next figure.



Figure 6.4: *Response to step reference and step input disturbance*

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# Lead-lag Compensators

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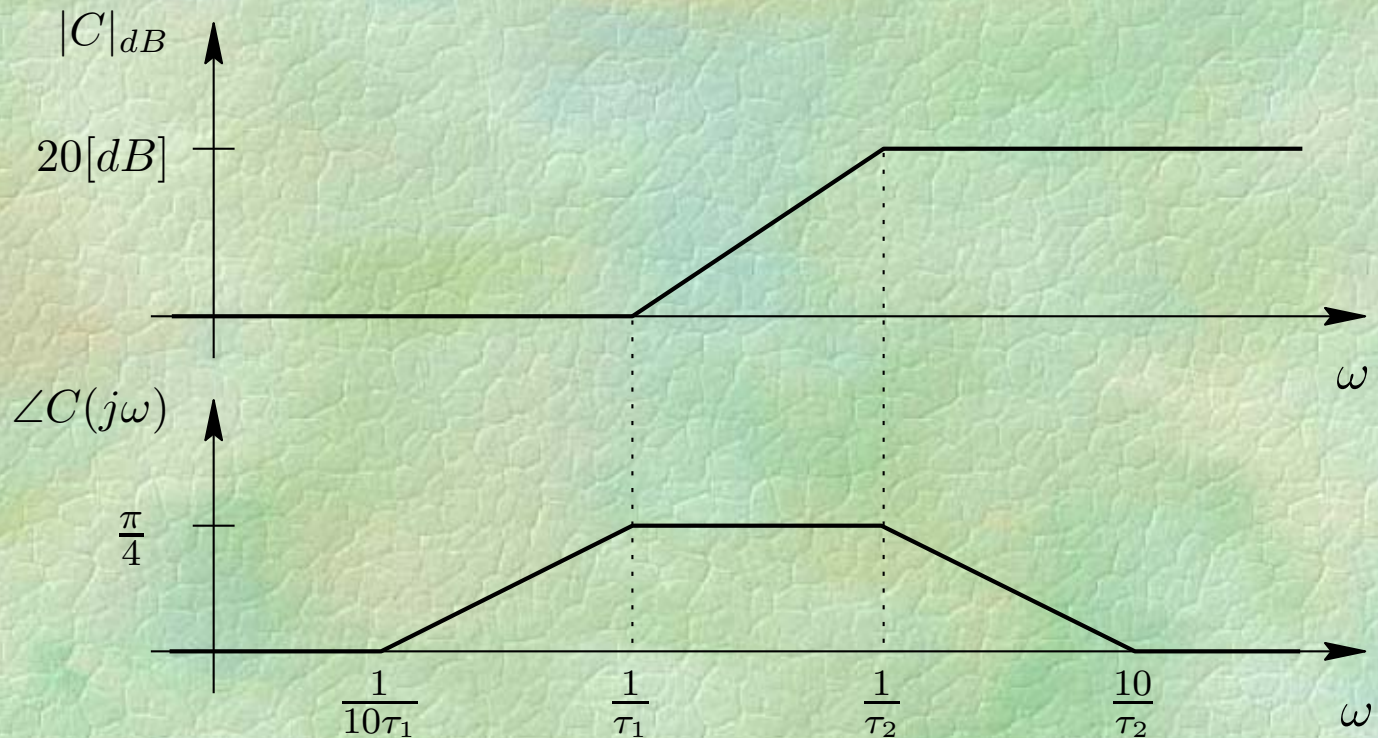
Closely related to PID control is the idea of lead-lag compensation. The transfer function of these compensators is of the form:

$$C(s) = \frac{\tau_1 s + 1}{\tau_2 s + 1}$$

If  $\tau_1 > \tau_2$ , then this is a *lead network* and when  $\tau_1 < \tau_2$ , this is a *lag network*.



Figure 6.9: *Approximate Bode diagrams for **lead networks** ( $\tau_1 = 10\tau_2$ )*





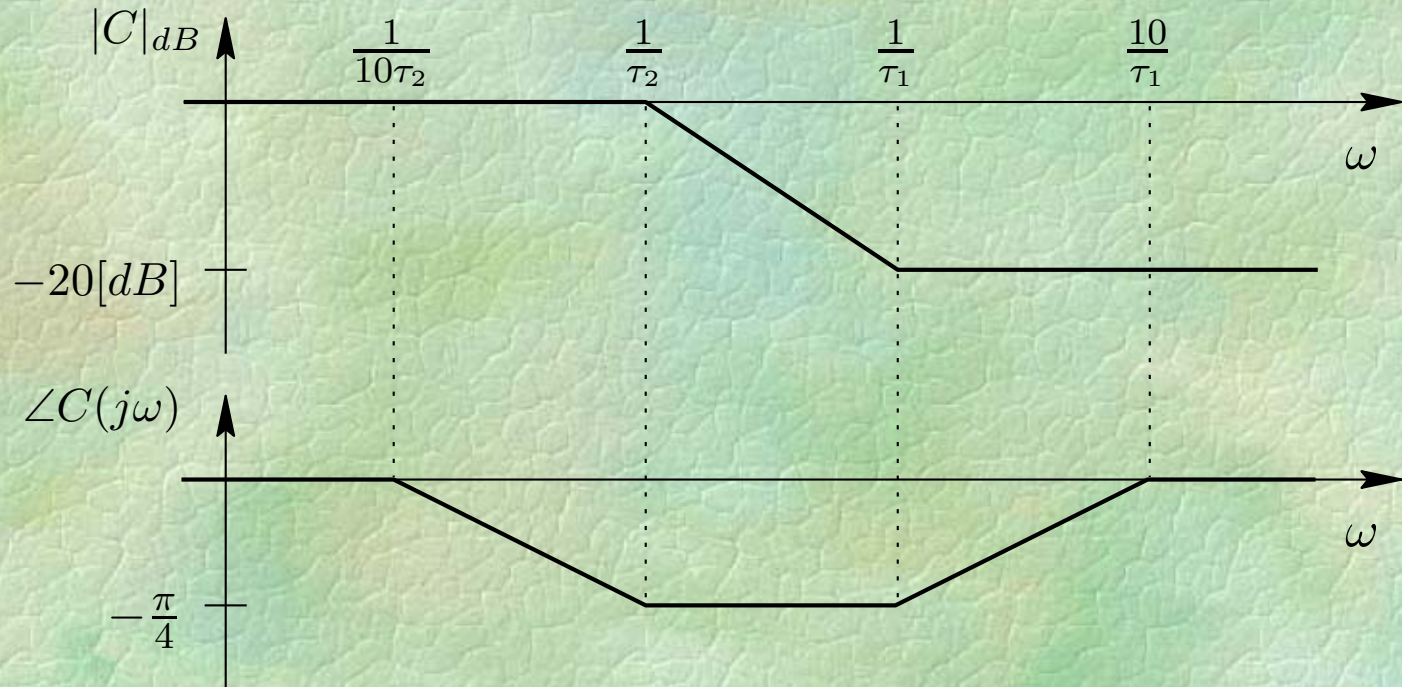
# Observation

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We see from the previous slide that the lead network gives **phase advance** at  $\omega = 1/\tau_1$  **without an increase in gain**. Thus it plays a role similar to **derivative action** in PID.



Figure 6.10: *Approximate Bode diagrams for lag networks* ( $\tau_2=10\tau_1$ )





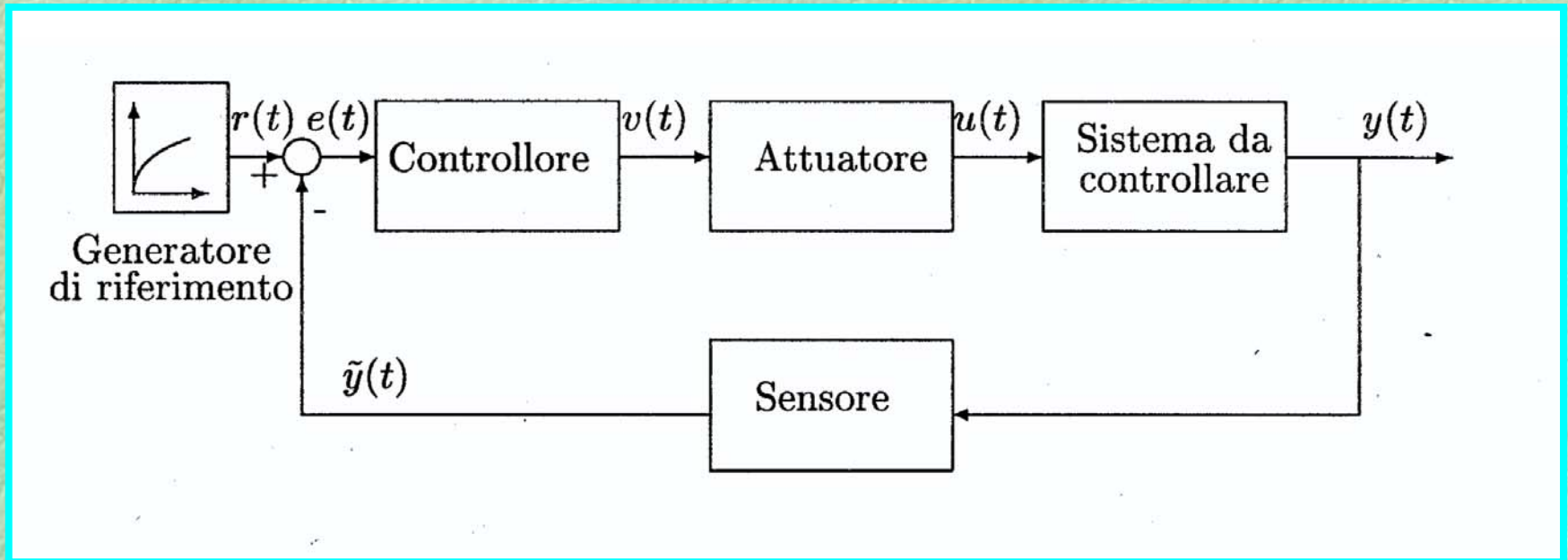
# Observation

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We see from the previous slide that the **lag network gives low frequency gain increase**. Thus it plays a role similar to integral action in PID.



# Industrial Controllers



**General controlled system structure**



# PID Functional Blocks

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$$u(t) = K \left( e(t) + \frac{1}{T_i} \int_0^t e(\tau) d\tau + T_d \frac{de(t)}{dt} \right)$$

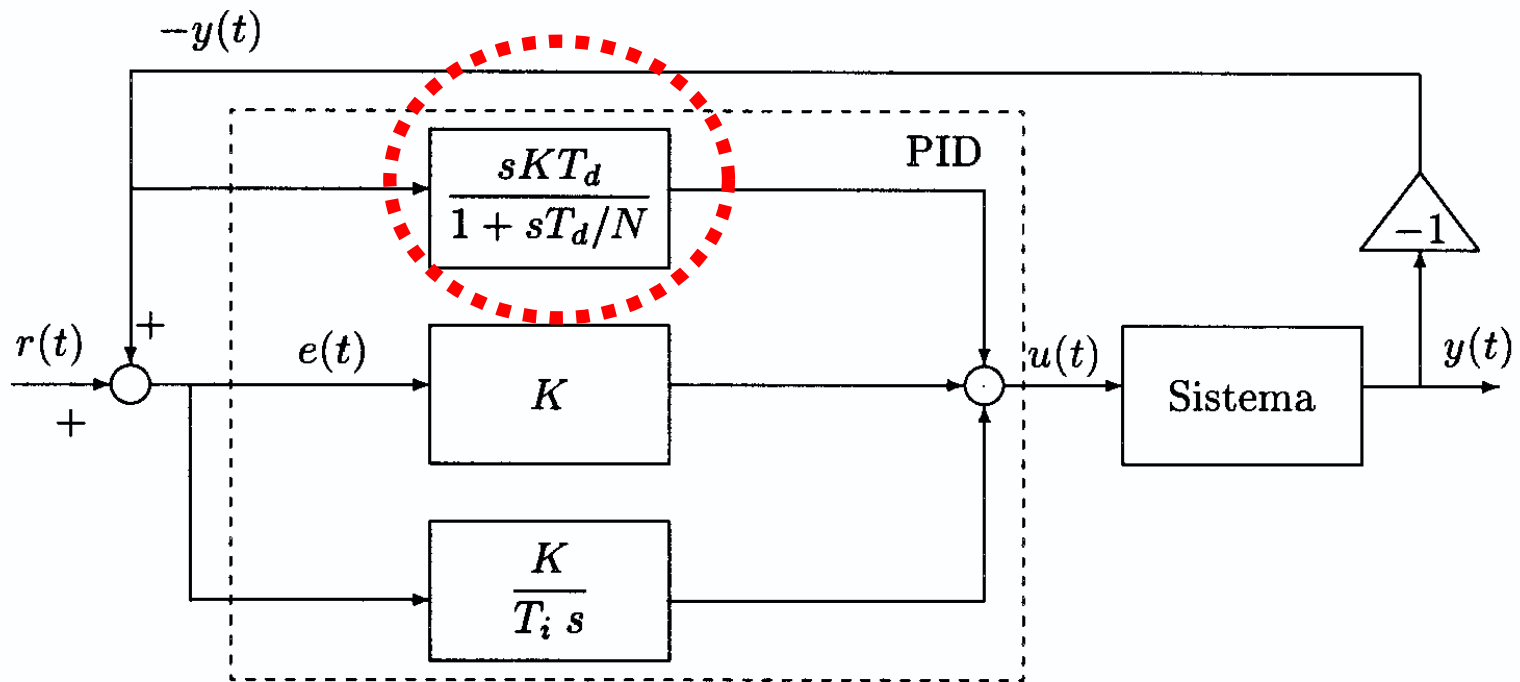
**But... Unfeasible controller!!!**

$$D(S) = \frac{sKT_d}{1 + sT_d/N}$$

**Feasible derivative contribution**



# “Real” PID Controller





# Continuous Time Controller Designs

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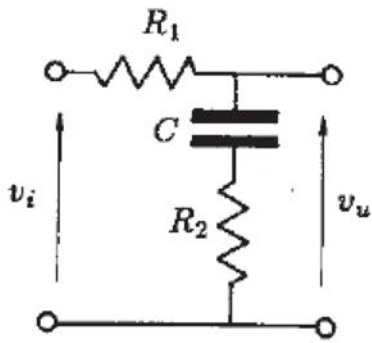
*Tools:*

*Bode Diagrams*

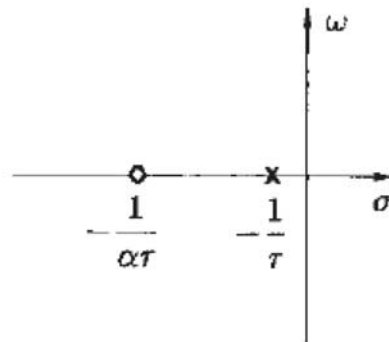
*Nichols Charts*



# Lag Network Example

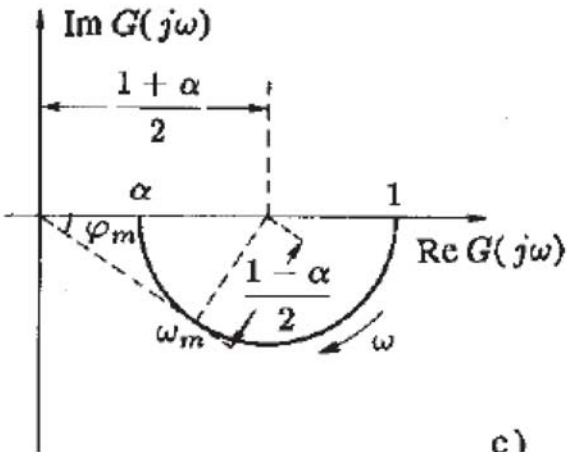


a)

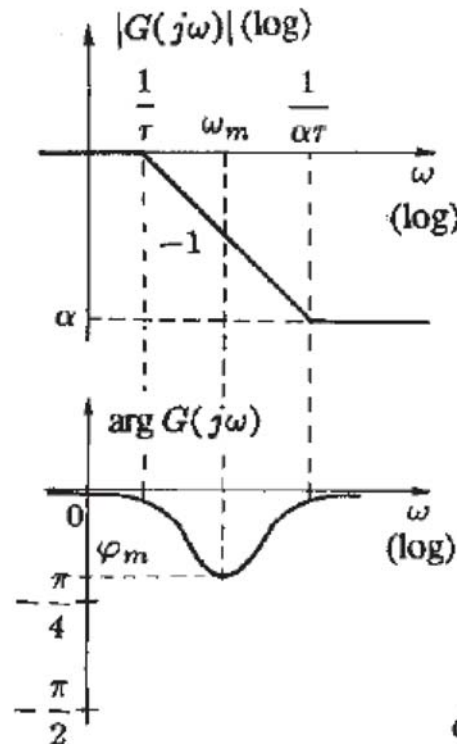


b)

$$G(s) = \frac{R_2 + \frac{1}{Cs}}{R_1 + R_2 + \frac{1}{Cs}} = \frac{1 + R_2 Cs}{1 + (R_1 + R_2)Cs} = \frac{1 + \alpha \tau s}{1 + \tau s}$$



c)

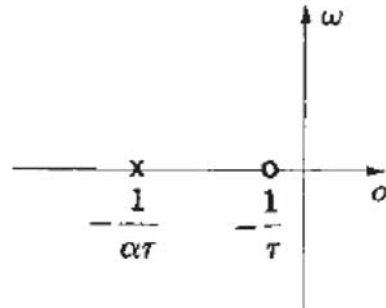
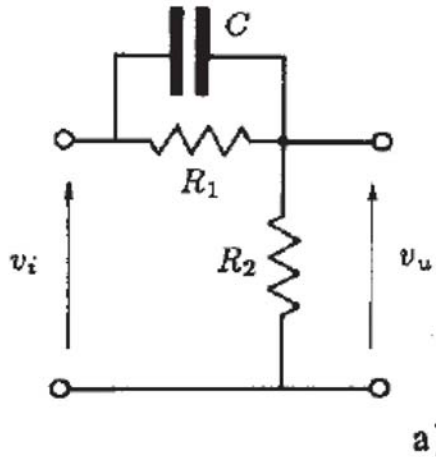


d)

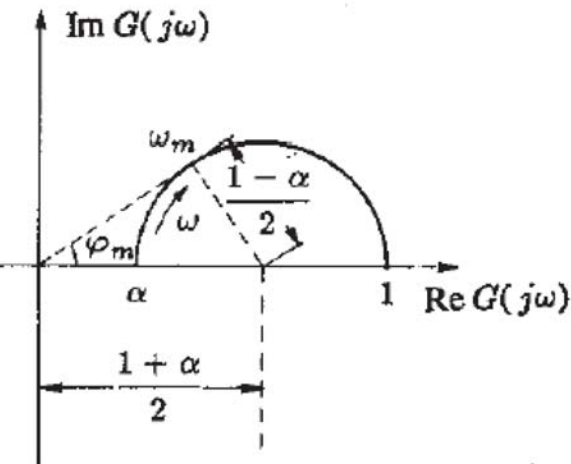
$$\varphi_m = -\arcsin \frac{1 - \alpha}{1 + \alpha}, \quad \omega_m = \frac{1}{\tau \sqrt{\alpha}}$$



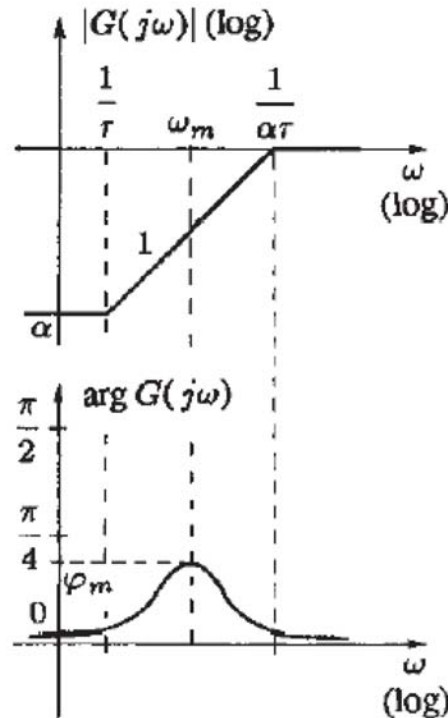
# Lead Network Example



$$G(s) = \frac{R_2}{R_2 + \frac{1}{(1/R_1) + Cs}} = \frac{R_2(1 + R_1Cs)}{R_1 + R_2 + R_1R_2Cs} = \alpha \frac{1 + \tau s}{1 + \alpha\tau s}$$



c)



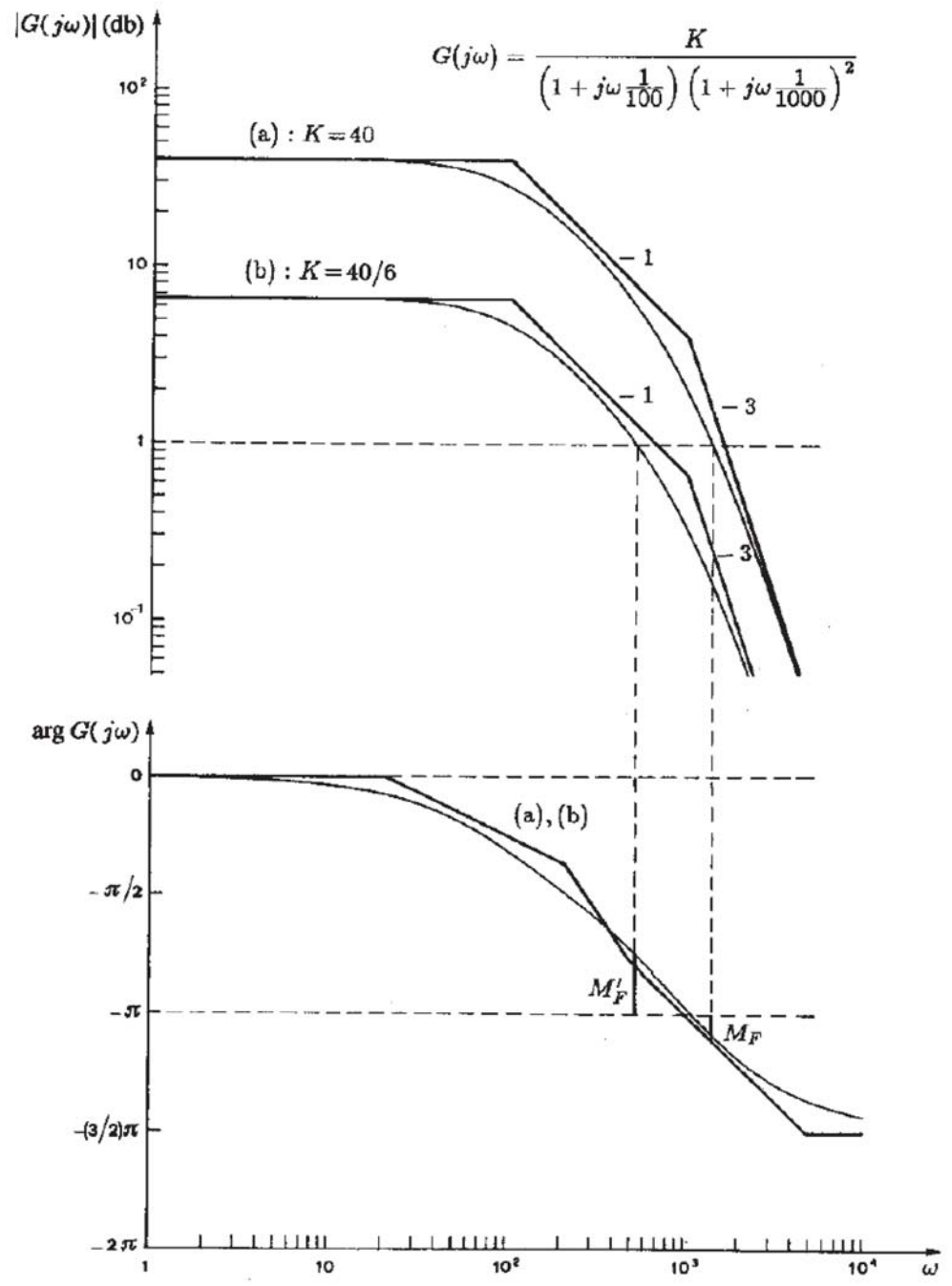
d)

$$\omega_m = \frac{1}{\tau\sqrt{\alpha}}$$

$$\varphi_m = \arcsen \frac{1 - \alpha}{1 + \alpha}$$

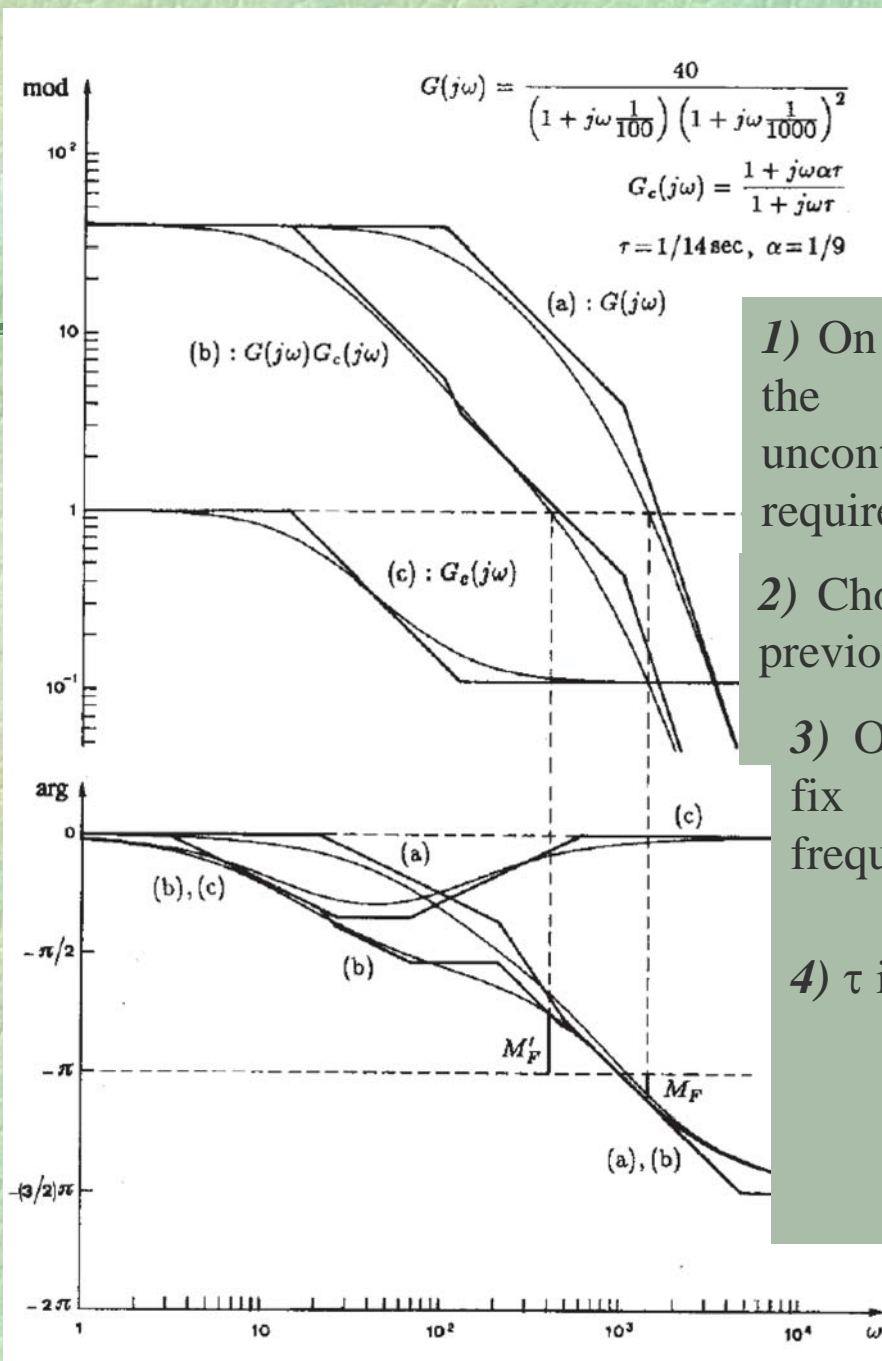


# Proportional Controller



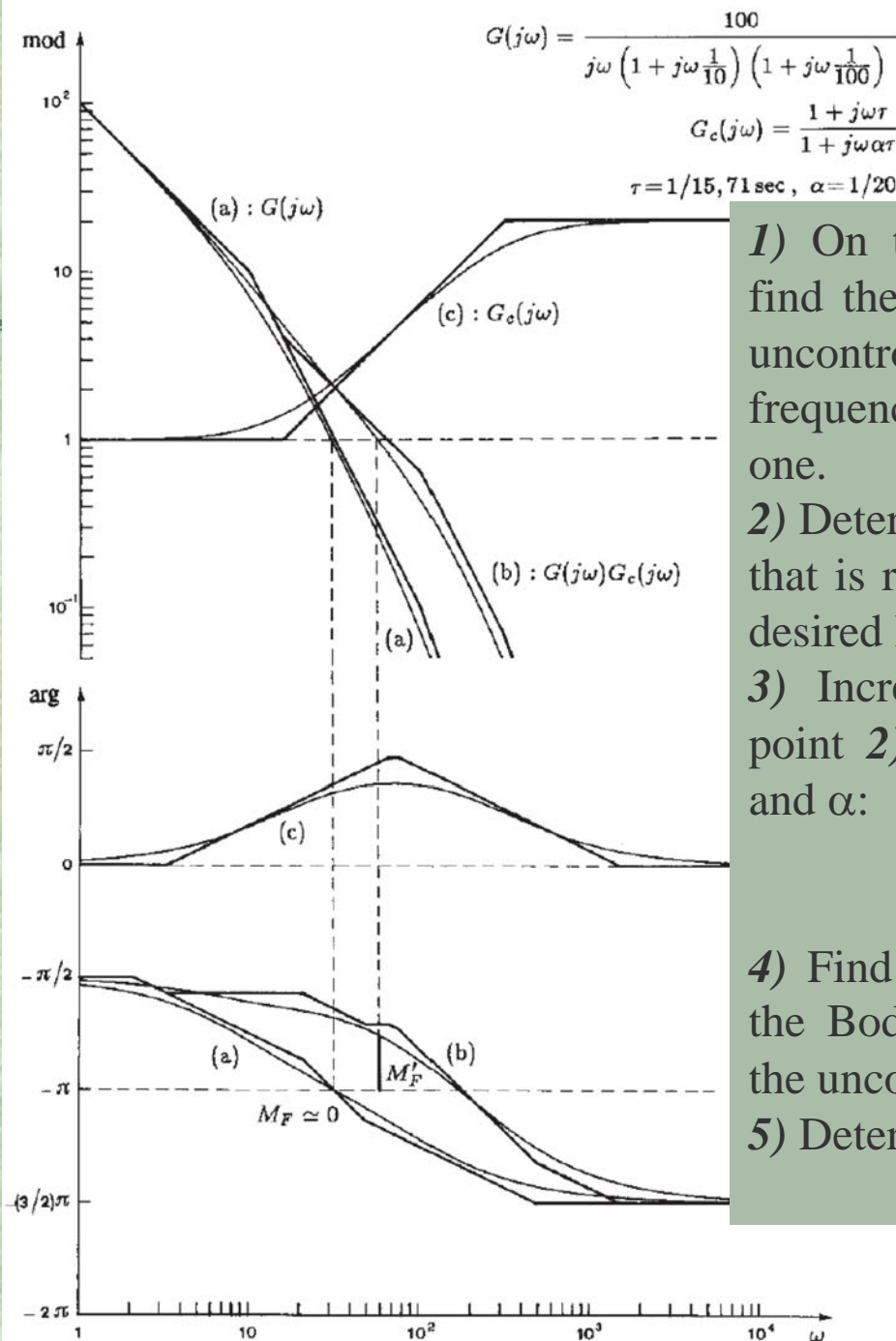


# Lag network controller



- 1) On the Bode phase diagram fix the frequency where the uncontrolled system has the required  $M_F$ .
- 2) Choose  $\omega^*$  20% less than the previous fixed frequency.
- 3) On the Bode magnitude plot fix the attenuation at the frequency  $\omega^*$  (i.e. the value of  $\alpha$ ).
- 4)  $\tau$  is computed by the relation:
 
$$\frac{1}{\alpha \tau} = \frac{\omega^*}{10}$$

# Lead network controller



- 1) On the Bode phase diagram find the phase margin  $M_f$  of the uncontrolled system and the  $\omega^*$  frequency where its magnitude is one.
- 2) Determine the basic phase lead that is required for achieving the desired  $M_f$ .
- 3) Increase the value fixed at point 2) and thus determine  $\phi_m$  and  $\alpha$ :
 
$$\alpha = \frac{1 - \sin(\phi_m)}{1 + \sin(\phi_m)}$$
- 4) Find the frequency  $\omega^*$  where the Bode magnitude diagram of the uncontrolled model is  $\alpha/2$ .
- 5) Determine  $\tau$  from the relation:

$$\omega^* = \frac{1}{\tau\sqrt{\alpha}} \quad 25/28$$



# Summary

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- y PI and PID controllers are widely used in industrial control.
- y From a modern perspective, a PID controller is simply a controller of (up to second order) containing an integrator. Historically, however, PID controllers were tuned in terms of their **P**, **I** and **D** terms.
- y It has been empirically found that the PID structure often has sufficient flexibility to yield excellent results in many applications.



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- y The basic term is the proportional term, **P**, which causes a corrective control actuation proportional to the error.
  - y The integral term, **I** gives a correction proportional to the integral of the error. This has the positive feature of ultimately ensuring that sufficient control effort is applied **to reduce the tracking error to zero**. However, integral action tends to have a **destabilizing effect** due to the increased phase shift.



- y The derivative term, **D**, gives a predictive capability yielding a control action proportional to the rate of change of the error. This tends to have a **stabilizing effect but often leads to large control movements**.
- y Various empirical tuning methods can be used to determine the PID parameters for a given application. They should be considered as a first guess in a search procedure.